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ИЗВОД

ИЗРАЧУНАВАЊЕ ТЕОРИЈОМ ФУНКЦИОНАЛА ГУСТИНЕ МЕХАНИЗМА КРЕКОВАЊА
ПРОПАНА НА ХРОМ (III) ОКСИДУ КЛАСТЕРСКИМ ПРИСТУПОМ

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Таложeње кокса на катализатору и производња нежељених производа током трансформисања пропана у пропилен представља велики изазов индустријском приступу производње пропилена. Механизам што доприноси овом изазову је теоријски проучаван преко изучавања реакционих путева крекковања да би се разумело како унапредити коксовање катализатора. Спроведена студија користећи DFT и кластерски приступ у потрази за кинетичким и термодинамским подацима реакционог механизма који је присутан у процесима на Cr₂O₃. Идентификовани су ступањ који одређује брзину реакције (RDS) и могући путеви који лако омогућавају производњу малих угљоводоника као што су етилен, метан и многи други. Студија сулфидне, супституицију Cr-места или додавање кисеоника, као начин да се побољша кинетика реакције, укључује дубоку дехидрогенацију код конверзије пропана у пропилен. Ова информација ће помоћи да се побољша перформанса Cr₂O₃ катализатора и даље побољша принос производа.

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SUPPLEMENTARY MATERIAL TO
**Density functional theory calculation of propane cracking
 mechanism over chromium (III) oxide by cluster approach**

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List of relevant models employed in this study

a) Enthalpy contributions

$$H_{\text{linear}}(T) = \left[\frac{5}{2} RT \right]_{\text{trans}} + [RT]_{\text{rot}} + \left[RT \sum_i \frac{h\nu_i}{k_B T} \frac{e^{-\frac{h\nu_i}{k_B T}}}{1 - e^{-\frac{h\nu_i}{k_B T}}} \right]_{\text{vib}} \quad (1)$$

$$H_{\text{non-linear}}(T) = \left[\frac{5}{2} RT \right]_{\text{trans}} + \left[\frac{3}{2} RT \right]_{\text{rot}} + \left[RT \sum_i \frac{h\nu_i}{k_B T} \frac{e^{-\frac{h\nu_i}{k_B T}}}{1 - e^{-\frac{h\nu_i}{k_B T}}} \right]_{\text{vib}} \quad (2)$$

$$\text{ZPE} = \frac{1}{2} \sum v_{n,i} \quad (3)$$

b) Entropy Contributions

$$s_{\text{linear}}(T) = R \left[\ln \frac{\{(2\pi m / h^2)\}^{\frac{3}{2}} (k_B T)^{\frac{5}{2}}}{P_0} + \frac{5}{2} \right]_{\text{trans}} + R \left[\ln \frac{8\pi^2 k_B T I_r, \text{linear}}{h^2 \rho_r} + 1 \right]_{\text{rot}} + \left[R \sum_i \frac{\frac{h\nu_i}{k_B T}}{e^{\frac{h\nu_i}{k_B T}} - 1} - R \sum_i \ln \left(1 - e^{-\frac{h\nu_i}{k_B T}} \right) \right]_{\text{vib}} \quad (4)$$

$$s_{\text{non-linear}}(T) = R \left[\ln \frac{(2\pi m / h^2)^{\frac{3}{2}} (k_B T)^{\frac{5}{2}}}{P_0} + \frac{5}{2} \right]_{\text{trans}} +$$

$$R \left[\ln \frac{8\pi^2 (2\pi k_B)^{\frac{3}{2}} (T)^{\frac{3}{2}} (I_a I_b I_c)^{\frac{1}{2}}}{h^3 \rho_r} + \frac{3}{2} \right]_{\text{rot}} +$$

$$\left[R \sum_i \frac{\frac{h\nu_i}{k_B T}}{e^{\frac{h\nu_i}{k_B T}} - 1} - R \sum_i \ln \left(1 - e^{-\frac{h\nu_i}{k_B T}} \right) \right]_{\text{vib}} \quad (5)$$

$$S_{\text{config}} = R \left[\ln \left(\frac{1-\theta}{\theta} \right) - \frac{\ln(1-\theta)}{\theta} \right] \quad (6)$$

$$S_{\text{config}} = 1.39 R \quad (7)$$

TABLE S-I. The activation and reaction energies across Cr-Cr, Cr-O sites for scheme S1.

Step	E_a / eV				$\Delta G / \text{eV}$			
	CrCr-S1		CrO-S1		CrCr-S1		CrO-S1	
	F	R	F	R	F	R	F	R
ads	-0.37	0.37	-0.37	0.37	-0.37	0.37	-0.37	0.37
suf	0.54	0.18	0.54	0.18	0.36	-0.36	0.36	-0.36
diff	-0.53	0.53	-0.53	0.53	-0.53	0.53	-0.53	0.53
cra1	0.17	0.77	0.22	0.80	-0.60	0.60	-0.58	0.58
cra2	0.52	-0.52	0.58	-0.58	0.52	-0.52	0.58	-0.58
des	0.25	-0.25	0.19	-0.19	0.25	-0.25	0.19	-0.19

TABLE S-II. The activation and reaction energies across Cr-Cr, Cr-O sites for scheme S2.

Step	E_a / eV				$\Delta G / \text{eV}$			
	CrCr-S2		CrO-S2		CrCr-S2		CrO-S2	
	F	R	F	R	F	R	F	R
Ads	-0.37	0.37	-0.37	0.37	-0.37	0.37	-0.37	0.37
Suf	0.70	0.45	0.72	0.38	0.26	-0.26	0.34	-0.34
Diff	-0.45	0.45	-0.48	0.48	-0.45	0.45	-0.48	0.48
cra1	0.28	0.86	0.24	0.85	-0.58	0.58	-0.61	0.61
cra2	0.52	-0.52	0.58	-0.58	0.52	-0.52	0.58	-0.58
des	0.25	0.25	0.19	0.25	0.25	-0.25	0.19	-0.19

TABLE S-III. Free energies of the species computed

Species	Chemical formula	Symbols	H° / eV	$S^\circ / \text{eV K}^{-1}$	G° / eV
1 st Dehy. CrCr	TS (C ₃ H ₇ *H)	TS11	3.1223	0.0017	2.6166
1 st Dehy. CrO	TS (C ₃ H ₇ *H)	TS12	2.9888	0.0016	2.5210
1 st Dehy. CrCr	TS (C ₃ H ₇ *H)	TS21	3.1213	0.0015	2.6845
1 st Dehy. CrO	TS (C ₃ H ₇ *H)	TS22	3.1076	0.0014	2.6985
Cracking of propyl-1, CrCr	TS (C ₂ H ₄ *CH ₃)	TScp1CrCr	2.7798	0.0016	2.2955
Cracking of propyl-1, CrO	TS (C ₂ H ₄ *CH ₃)	TScp1CrO	2.7942	0.0015	2.3414
Cracking of propyl-2, CrCr	TS (C ₂ H ₄ *CH ₃)	TScp2CrCr	2.8599	0.0016	2.3795
Cracking of propyl-2, CrO	TS (C ₂ H ₄ *CH ₃)	TScp2CrO	2.7539	0.0012	2.3903
H Diff., CrO	TS (H*CH ₃)	TS_Cat_Cr(M)O(H)_o	1.4611	0.0012	1.1083
Methane	CH ₄	M	1.3356	0.0021	0.7112
Cracking of methyl, Cr	TS (H*CH ₂)	TS_Cat_Cr(M)	1.3292	0.0008	1.0794
Cracking of methyl, O	TS (H*CH ₂)	TS_Cat_O(M)	1.0145	0.0012	0.6684

TABLE IV. Free energies of the species computed (Note: "*" signifies that it is surface specie)

Species	Chemical formula	Symbols	H° / eV	$S^\circ / \text{eV K}^{-1}$	G° / eV
Catalyst	Cr ₂ O ₃	X	0.3390	0.00031	0.2450
Propane	C ₃ H ₈	R	2.9814	0.0029	2.1062
Phys. Propane	*C ₃ H ₈	RX	3.4571	0.0049	1.9828
Propyl-1&H, CrCr	CH ₃ CH ₂ CH ₂ **H	UHX11	3.2556	0.0033	2.2601
Propyl-1&H, CrO	CH ₃ CH ₂ CH ₂ **H	UHX12	3.3686	0.0034	2.3418
Propyl-2&H, CrCr	CH ₃ CH*CH ₃ H	UHX21	3.2461	0.0034	2.2392
Propyl-2&H, CrO	CH ₃ CH*CH ₃ *H	UHX22	3.3644	0.0035	2.3234
Hydrogen, Cr	*H	HX1	0.5841	0.0023	-0.1063
Hydrogen, O	*H	HX2	0.6949	0.0025	-0.0611
Propyl-1, CrCr	CH ₃ CH ₂ CH ₂ *	UX11	3.0783	0.0032	2.1216
Propyl-1, CrO	CH ₃ CH ₂ CH ₂ *	UX12	3.1534	0.0033	2.1625
Propyl-1, OCr	CH ₃ CH ₂ CH ₂ *	UX21	3.0740	0.0033	2.0991
Propyl-1, OO	CH ₃ CH ₂ CH ₂ *	UX22	3.1344	0.0033	2.1509
Hydrogen gas	H ₂	H2	0.3661	0.0015	-0.0857
Ethylene	C ₂ H ₄	ET	1.5018	0.0024	0.7760
Methyl, CrO	*CH ₃	Cat_cr(M)_o	1.4670	0.0028	0.6443
Ethylene, CrCr	*C ₂ H ₄	Cat_Cr(Ey)Cr_o	1.9491	0.0028	1.1235
Ethylene, CrO	*C ₂ H ₄	Cat_O(Ey)Cr_o	1.9828	0.0028	1.1400
Methyl & H, OO	H*CH ₃	Cat_O(M)O(H)_o	1.7226	0.0030	0.8273
Methyl & H, CrO	H*CH ₃	Cat_Cr(M)O(H)_o	1.7482	0.0030	0.8671
H Diff., CrO	TS (H*CH ₃)	TS_Cat_Cr(M)O(H)_o	1.4611	0.0012	1.1083
Methane	CH ₄	M	1.3356	0.0021	0.7112
Methylene, Cr	CH ₂	Cat_Cr(My)Cr	1.1254	0.0027	0.3339
Methylene, O	CH ₂	Cat_O(My)Cr	1.1671	0.0027	0.3595